

SDMS Document ID



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EPA NO. U590002

FILE NO. PZ-8

**PROCESS FLOWCHARTS
AND
DETAILED DESCRIPTIONS**

Attachment G

Information Request #4

April 19, 1990

APEX MILL FLOWSHEET DESCRIPTION

The ore from the Apex mine is transported by truck to the Apex mill. There it is stockpiled until required for feed. The ore is moved from the stockpile by front end loader where it enters the grinding circuit.

Grinding

Prior to shipment to the mill, the ore is crushed to 3/4 inch in diameter. At the mill, the ore is ground wet in a ball mill using steel grinding balls. The discharge from the grinding mill is screened, with the oversize particles returning to the mill, and the fine particles passing to the next step. After passing the grinding-screening step ore particles are less than 0.01 inch diameter.

Carbonate Removal

The ore contains 6% carbonate in the form of calcite (CaCO_3) and dolomite (MgCO_3). Because the carbonate interferes with the subsequent beneficiation steps it is removed by giving the ore an acid wash. This is accomplished in a large agitation tank to which a weak solution of sulfuric acid is added.

1st Stage Leach

After carbonate removal the ore enters the first stage leach circuit. This circuit consists of 17 tanks arranged for series flow. Sulfuric acid is added to the first 14 tanks to maintain an acid strength of 30 g/l H_2SO_4 . Sulfur dioxide is also added to assist in the leaching. No acid or sulfur dioxide is added to the last three tanks allowing acid concentration to drop to less than 20 g/l H_2SO_4 .

Most of the germanium is leached in the first stage leach circuit.

Thickener No. 1

Thickener No. 1 is a settling vessel which receives the discharge from the first stage leach circuit. The solids settle to the bottom of the vessel and are pumped to second stage leach circuit. The clear liquid overflows the vessel and goes to the gypsum precipitation circuit.

2nd Stage Leach

The second stage leach circuit is a series of five agitation tanks. The solids from Thickener No. 1 are mixed with sulfuric acid and sulfur dioxide. The acid concentration is 70-90 g/l H_2SO_4 .

The remainder of soluble germanium is leached in the second stage leach circuit.

Thickener No. 2

Thickener No. 2 receives the discharge from the second stage leach circuit. The solids settle and are pumped to the third stage leach circuit. The clear liquid overflow is returned to first stage leach circuit.

3rd Stage Leach

The third stage leach circuit is a series of three agitation tanks. The solids from thickener No. 2 are mixed with sulfuric acid at a concentration of 300 g/l H₂SO₄.

Much of the gallium is leached from the ore in this stage.

Thickener No. 3

Thickener No. 3 receives the discharge from the third stage leach circuit. The solids are settled and pumped to the belt filter. The liquid overflow is returned to the second stage leach circuit.

Belt Filter and Repulp

The belt filter is a horizontal vacuum filter. The solids from thickener No. 3 are filtered and washed, after which they are reslurried with water. These tailings are then pumped to a neutralization circuit. The filtrate and the wash liquid are returned to thickener No. 3.

Gypsum Precipitation

The liquid overflowing thickener No. 1 contains germanium, gallium, and copper as well as impurities. One of the impurities is gypsum. By holding the solution for an extended period of time in a quiet tank much of the gypsum settles out and can be removed. This gypsum removal operation reduces problems downstream.

Clarifier

The clarifier is a second settling tank which allows additional time for gypsum and other solids to settle and be removed.

Copper Solvent Extraction

The copper solvent extraction circuit is a system of agitation tanks and settlers. Here the clarified leach solution is mixed with an organic liquid,

which has an affinity for copper. The copper is removed from the leach solution and eventually is isolated in an acid solution. The leach solution, which remains after the copper extraction step, goes to the gallium solvent extraction circuit.

Copper Electrowinning

The acid solution containing the copper is pumped to a copper electrowinning circuit. Here the copper is plated, electrolytically, to stainless steel cathodes. The copper plates are periodically stripped, packaged, and sold.

Gallium Solvent Extraction

The gallium solvent extraction circuit is similar to the copper circuit. An organic liquid with an affinity for gallium is used. The gallium is separated from germanium and the bulk of impurities in the leach solution. The leach solution, which remains after the gallium solvent extraction step, goes to the germanium solvent extraction circuit.

Gallium Purification and 2nd Solvent Extraction

In order to be marketable, gallium must be very pure. This is achieved in a series of purification steps including a second solvent extraction stage. The purification steps essentially remove all impurities from the gallium solution.

Gallium Electrowinning

Gallium metal is recovered from solution by electrowinning. The metal is collected, packaged and sold.

Germanium Solvent Extraction

The germanium solvent extraction circuit separates germanium from the remaining elements in the liquid. A combination of organic reagents with a strong affinity for germanium is used. The germanium is isolated with minor amounts of impurities in an alkaline solution.

Germanium Precipitation

Germanium is precipitated from the alkaline solution by neutralizing it with a sulfuric acid solution. The precipitate is sodium germanate, a white crystalline compound. Occasionally an excess of impurities will be co-precipitated with the sodium germanate. When this happens the sodium germanate is dissolved in a caustic solution and re-precipitated.

The sodium germanate is filtered from the liquid, dried, packaged and sold.

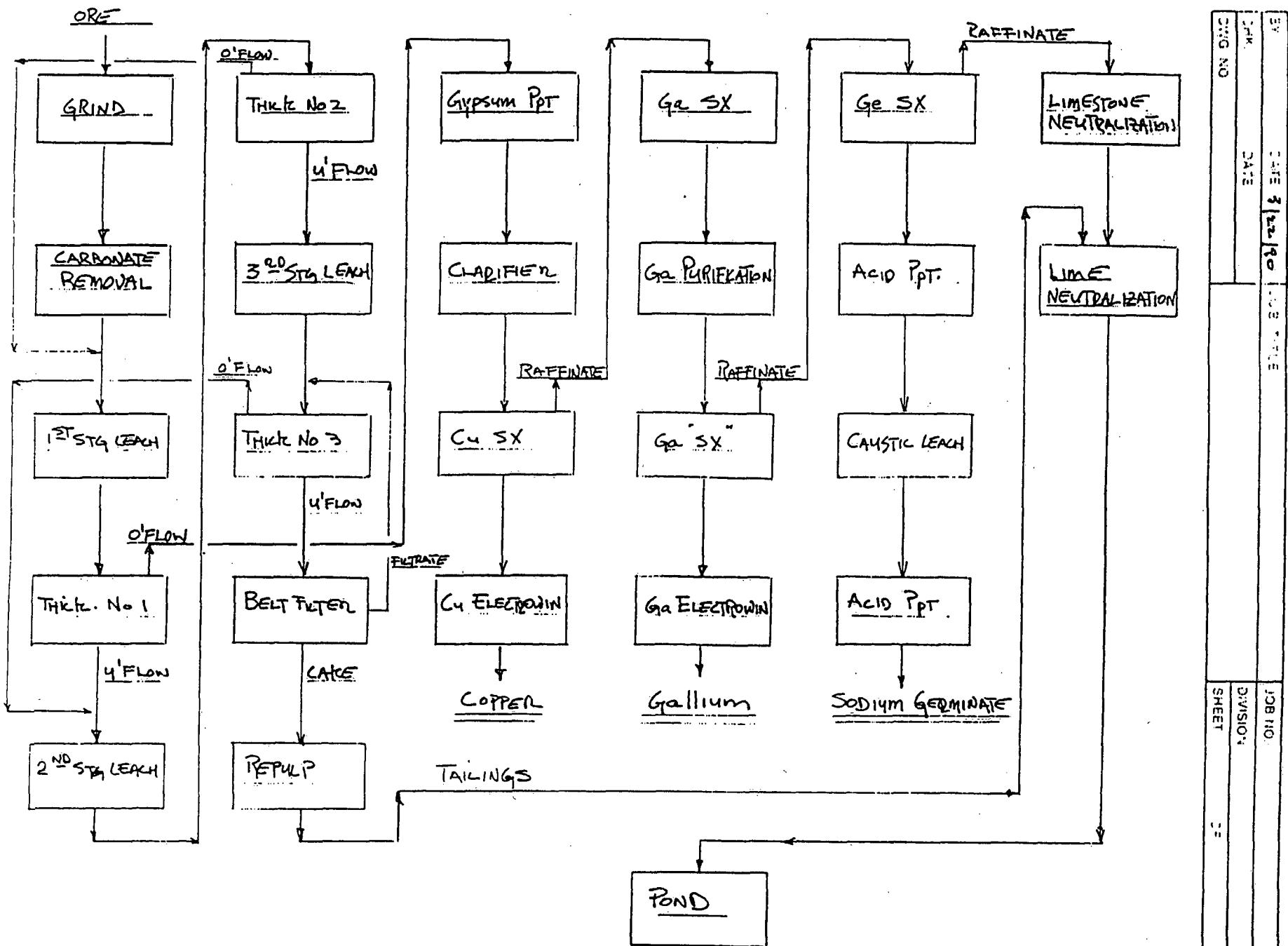
Neutralization Circuit

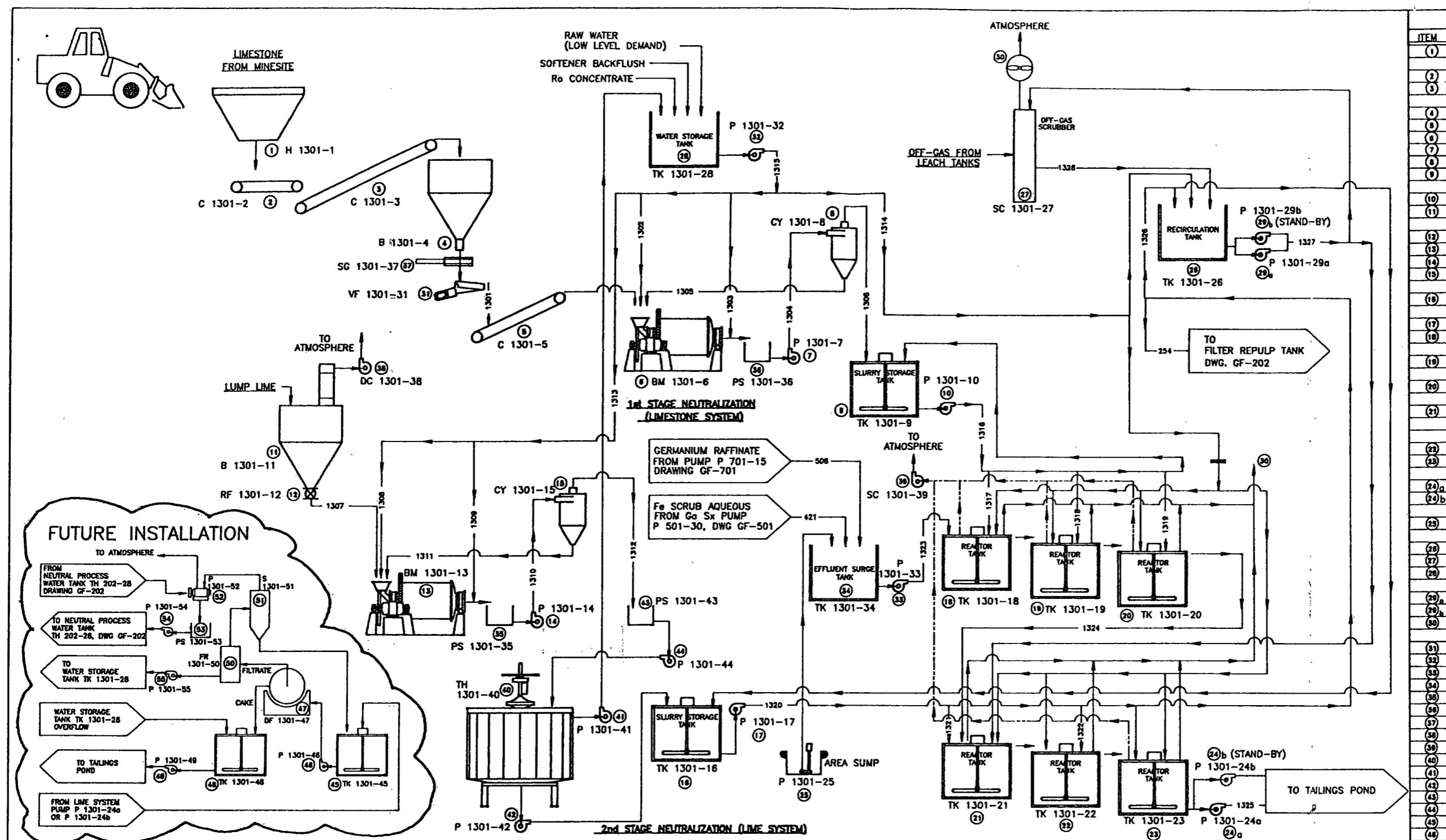
The leach solution which remains after the germanium precipitation step, is moderately acidic and contains heavy metals which were dissolved in the solution.

This solution is treated in the neutralization circuit. Limestone is used to destroy the acid, causing the pH to rise to 4.5. Slurried lime is then added to immobilize the heavy metals. The treated effluent is pumped to tailing ponds. Analyses to date indicate that this effluent does not exhibit any RCRA hazardous waste characteristics.

JDS:dld

APEX FLOWSHEET - SIMPLIFIED



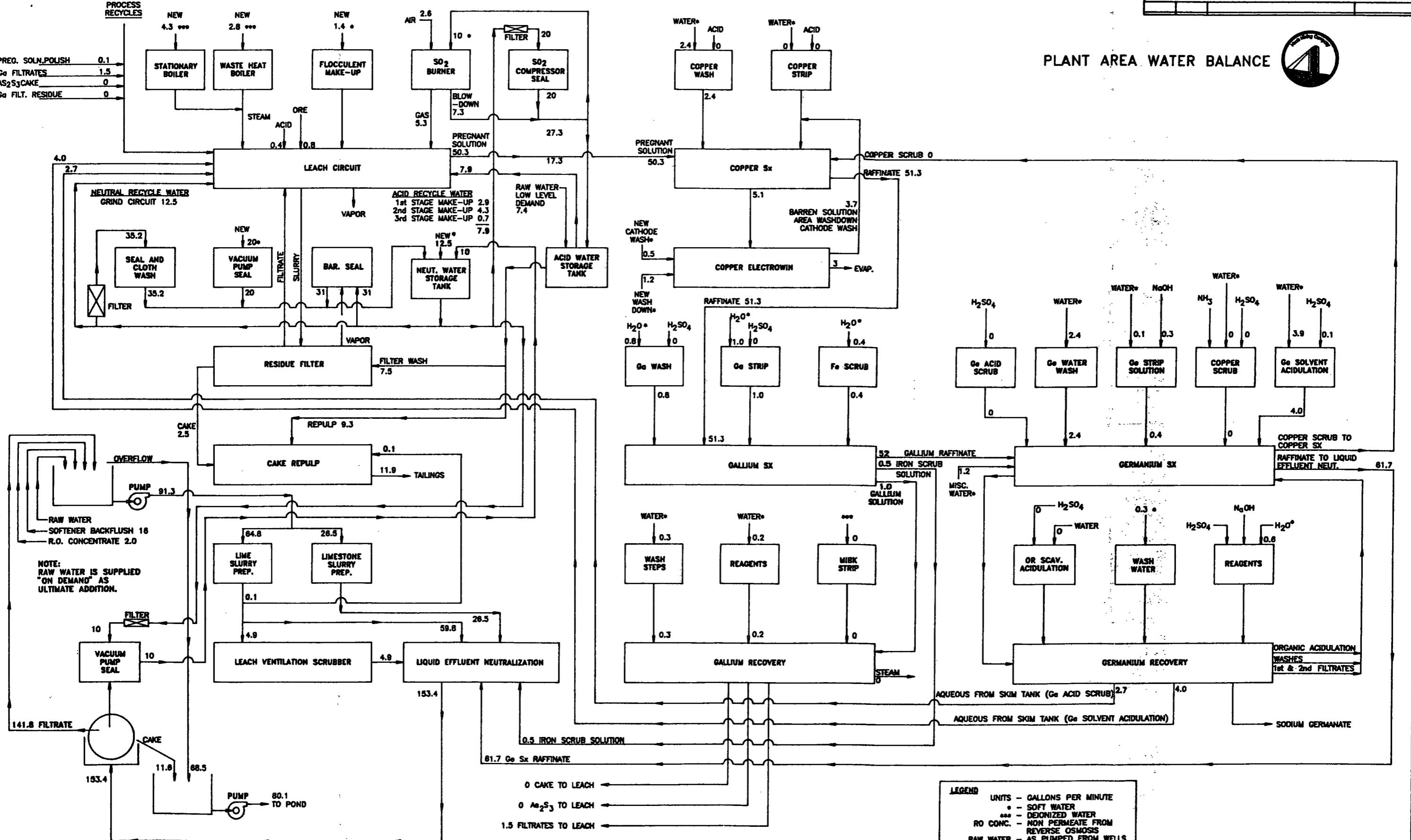


STREAM NUMBER	PHASE	SOLIDS LBS/HR	LIQUID LBS/HR	GAS LBS/HR	TOTAL LBS/HR	GPM	SG	H ₂ SO ₄ g/l
1301 LIMESTONE FEED	SOLID	8,400	538	-	8,938	-	2.7	70
1302 GRIND WATER	LIQUID	-	3,084	-	3,084	6.1	1.0	-
1303 DILUTION WATER	LIQUID	-	21,600	-	21,600	43.2	1.0	70
1304 CYCLONE FEED	SLURRY	25,200	32,400	-	57,600	63.5	1.36/44	70
1305 CYCLONE UNDERFLOW	SLURRY	16,800	7,200	-	24,000	28.8	1.79/70	70
1306 CYCLONE OVERFLOW	SLURRY	8,400	25,200	-	33,600	58.8	1.19/25	70
1307 LIME FEED	SOLID	3,600	-	-	3,600	-	2.3	70
1308 GRIND WATER	LIQUID	-	14,400	30.2	14,400	30.2	1.0	70
1309 DILUTION WATER	LIQUID	-	18,000	-	18,000	37.8	1.0	70
1310 CYCLONE FEED	SLURRY	5,400	34,200	-	39,600	73	1.08/13.8	<150
1311 CYCLONE UNDERFLOW	SLURRY	1,800	1,800	-	3,600	5	1.39/50.0	<150
1312 CYCLONE OVERFLOW	SLURRY	3,600	32,400	-	36,000	68	1.06/10.0	<150
1313 TOTAL WATER TO SLAGNO	LIQUID	-	32,400	-	32,400	68	1.0	70
1314 WATER TO SPRAYS & SCRUBBER	LIQUID	-	AS REQ'D	-	-	-	-	-
1315 TOTAL WATER TO NEUTRALIZATION	LIQUID	-	57,800	-	57,800	115	1.0	70
1316 LIMESTONE SLURRY DISTR.	SLURRY	6,800	19,800	-	26,400	44.5	1.19/25	70
1317 LIMESTONE TO 1st REAC.	SLURRY	1,470	4,410	-	5,880	9.9	1.19/25	70
1318 LIMESTONE TO 2nd REAC.	SLURRY	1,485	4,395	-	5,860	9.8	1.19/25	70
1319 LIMESTONE TO 3rd REAC.	SLURRY	1,465	4,395	-	5,860	9.9	1.19/25	70
1320 LIME DISTRIBUTION DISTR.	SLURRY	5,400	48,600	-	54,000	99.8	1.06/10	100
1321 LIME TO 4th REAC.	SLURRY	2,988	26,890	-	29,878	55.1	1.06/10	100
1322 LIME TO 5th REAC.	SLURRY	331	2,979	-	3,310	6.1	1.06/10	100
1323 EFFLUENT TO NEUTRALIZATION	LIQUID	-	36,352	62.2	36,352	62.2	1.17	80
1324 DISCHG. FROM LIMESTONE NEUT.	SLURRY	6,938	42,077	-	52,015	80.8	1.28	90
1325 DISCHARGE TO POND	SLURRY	13,531	74,412	-	87,943	151.8	1.18	100
1326 LIME TO SCRUBBER	SLURRY	274	2,466	-	2,740	5.1	1.06/10	100
1327 SCRUBBER RECIRCULATION	SLURRY	6,598	77,364	-	83,982	180	1.06/10	100
1328 SCRUBBER SUMP	SLURRY	6,870	70,930	-	88,700	165.1	1.06/10	100
1329 SCRUBBER EMISSION	GAS	-	-	-	-	-	-	-
1330 REAC. TANK EMISSION	GAS	-	-	1,934	1,934	260 scfm	-	100
1331 SCRUBBER BLEED	SLURRY	274	2,466	-	2,740	5.1	1.06/10	100
254 LIME TO LEACH RESIDUE	SLURRY	7	63	-	70	0.1	1.06/10	100

EQUIPMENT LIST			
ITEM	H.P.	DESCRIPTION	EQUIP. NO.
1	3 YD ³	FEED HOPPER	H 1301-1
2	3	24" x 8' BELT FEEDER	C 1301-2
3	5	18" x 84'L, BELT CONVEYOR	C 1301-3
4		230 TON LIMESTONE STORAGE BIN	B 1301-4
5		18" x 26'L BELT CONVEYOR	C 1301-5
6	50	5' x 5'H EIMCO BALL MILL	BM 1301-6
7	10	1 1/2" GALIGHER PUMP	P 1301-7
8		3" KREBS HYDROCYCLONE	CY 1301-8
9	5	TANK 8' x 8'H R.L. SLURRY STORAGE	TK 1301-9
10	5	1 1/2" GALIGHER PUMP	P 1301-10
11		200 TON LUMP LIME STORAGE BIN	B 1301-11
12	2	8" ROTARY FEEDER	RF 1301-12
13	10	30" x 36" DENVER BALL MILL	BM 1301-13
14	10	1 1/2" GALIGHER PUMP	P 1301-14
15		3" KREBS HYDROCYCLONE	CY 1301-15
16	5	TANK 8' x 8'H MS W/AGITATOR	TK 1301-16
17	10	1 1/2" GALIGHER PUMP	P 1301-17
18	3	12" x 15'H REACTOR W/AGITATOR	TK 1301-18
19	2	10" x 10'H FRP REACTOR WITH AGITATOR	TK 1301-19
20	2	10" x 10'H FRP REACTOR WITH AGITATOR	TK 1301-20
21	2	8" x 12'H REACTOR W/AGITATOR	TK 1301-21
22	2	8" x 8'H FRP REACTOR	TK 1301-22
23	2	8" x 8'H FRP REACTOR	TK 1301-23
24a	7.5	3" x 2' GOULDS PUMP	P 1301-24a
24b	7.5	3" x 2' GOULDS PUMP	P 1301-24b
25	5	1 1/2" GALIGHER SUM PUMP	P 1301-25
26		7" x 7'H RECIRCULATION TANK	TK 1301-26
27		OFF-GAS SCRUBBER	SC 1301-27
28	-	TANK 7" x 8'H FRP WATER STORAGE	TK 1301-28
29a	10	2" GALIGHER PUMP	P 1301-29c
29b	10	2" GALIGHER PUMP	P 1301-29b
30	10	SCRUBBER FAN (FURNISHED WITH SCRUBBER)	VF 1301-31
31	10	2" GOULDS PUMP - IRON	P 1301-32
32	1.5	1" GOULDS PUMP	P 1301-33
33	3	12" x 14'H FRP SURGE TANK	TK 1301-34
34		PUMP SUMP	PS 1301-35
35		PUMP SUMP	PS 1301-36
36		SLIDE GATE	SG 1301-37
37		BIN MOUNT DUST COLLECTOR	DC 1301-38
38		EXIST. 3 STAGE SCRUB. EXHAUST	SC 1301-39
39	2	THICKENER 20" x 12'	TH 1301-40
40	5	2" x 1 1/2" GALIGHER PUMP	P 1301-41
41	2	2" x 2" DORR PUMP	P 1301-42
42	AIR	PUMP SUMP	PS 1301-43
43		PUMP	P 1301-44
44		FUTURE TANK WITH AGITATOR	TK 1301-45
45		FUTURE PUMP	P 1301-46
46		FUTURE FILTER	DF 1301-47
47		FUTURE TANK WITH AGITATOR	TK 1301-48
48		FUTURE PUMP	P 1301-49
49		FUTURE FILTRATE RECIEVER	FR 1301-50
50		FUTURE BAROMETRIC SEPARATOR	S 1301-51
51		FUTURE VACUUM PUMP	P 1301-52
52		FUTURE SUMP PUMP	PS 1301-53
53		FUTURE PUMP	P 1301-54
54		FUTURE PUMP	P 1301-55
55		REVERSE	
56		REVERSE	
57		REVERSE	
58		REVERSE	
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BILL OF MATERIALS

PLANT AREA WATER BALANCE



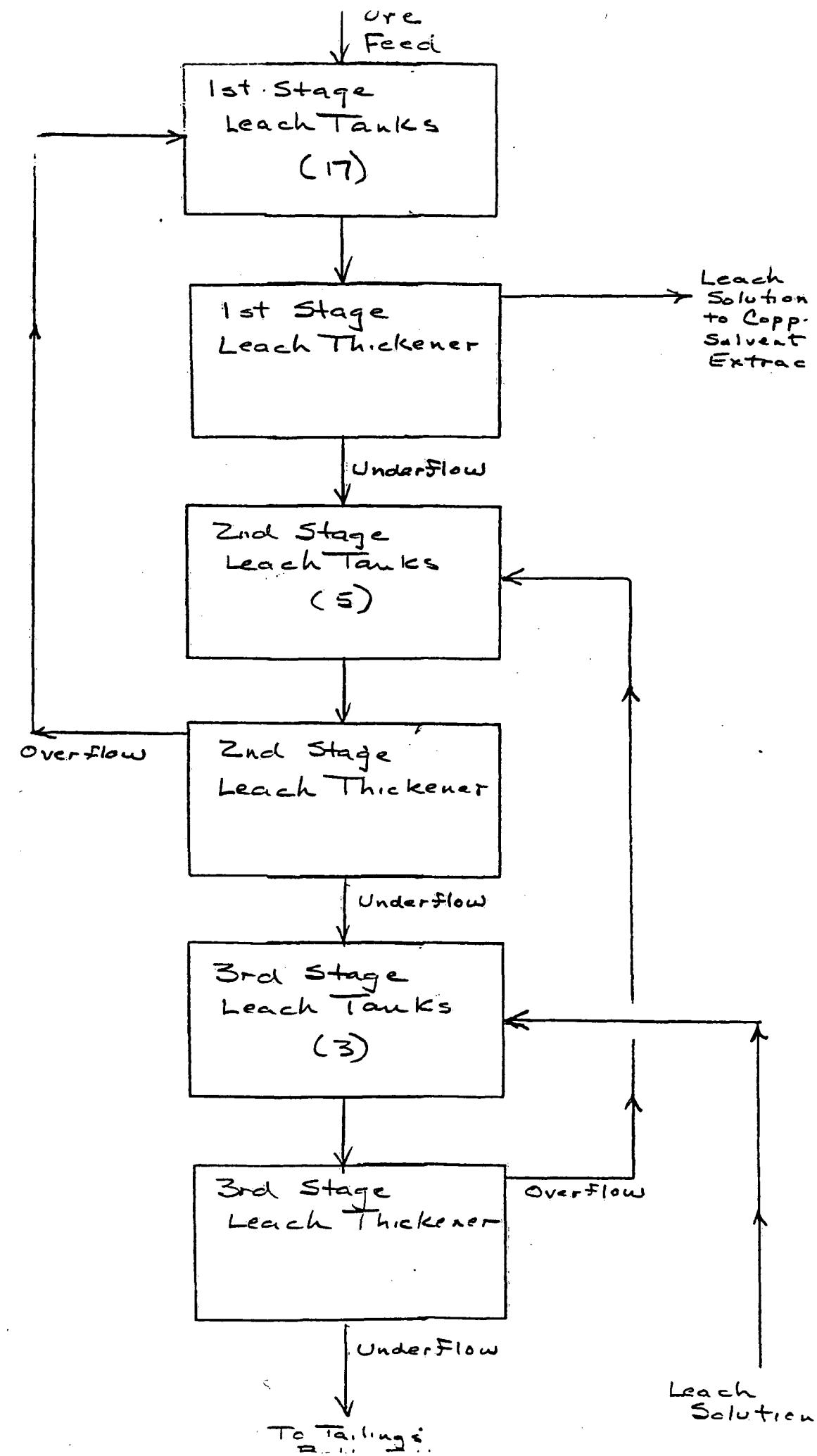
LEGEND

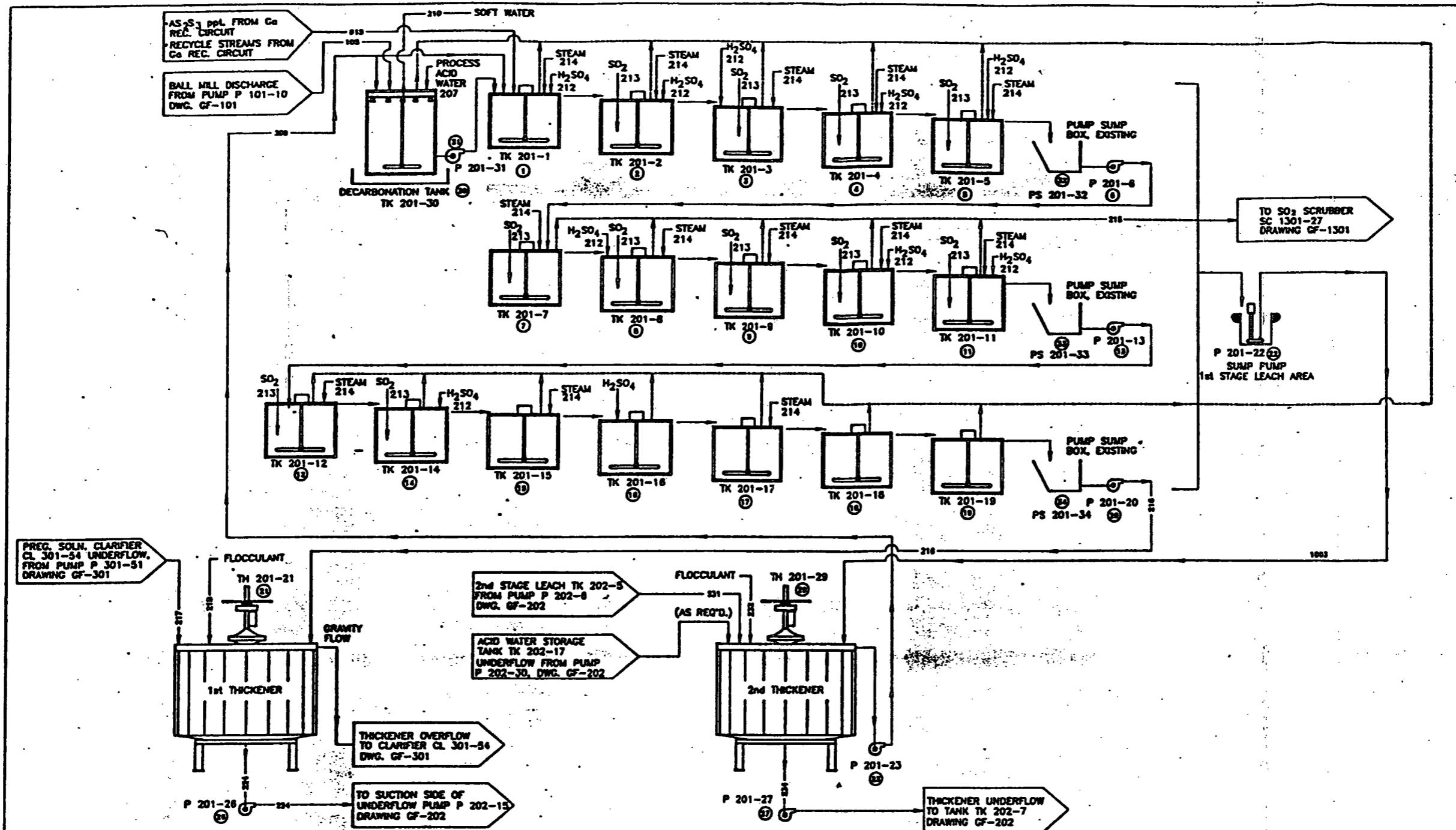
UNITS	- GALLONS PER MINUTE
•	- SOFT WATER
***	- DEIONIZED WATER
RO CONC.	- NON PERMEATE FROM REVERSE OSMOSIS
RAW WATER	- AS PUMPED FROM WELLS

1	2	3	4	5	6	7	8	9	10	11	12
DESCRIPTION	IN INCHES	TOLERANCES	INCHES	INCHES	INCHES	INCHES	INCHES				
HECLA MINING COMPANY						TOLERANCES ON DIMENSIONS, UNLESS OTHERWISE NOTED, ARE (PLUS OR MINUS) NON ACCUMULATIVE					
						0.010"					
						STRUCTURAL	1/16"				
						ALL DIMENS.	1/32"				
						APPROVED FOR CONSTRUCTION					
						DATE	11/2/69				
						SCALE	NO SCALE				

**Typical feedstock during Hecla Mining Company operations during the
Gallium/Germanium operations.**

Ga – 0.043%
Ge – 0.115%
Cu – 1.33%
Zn – 1.42%
Fe – 25.3%
As – 0.74%
SiO₂ – 45.5%
CO₂ – 1.61%

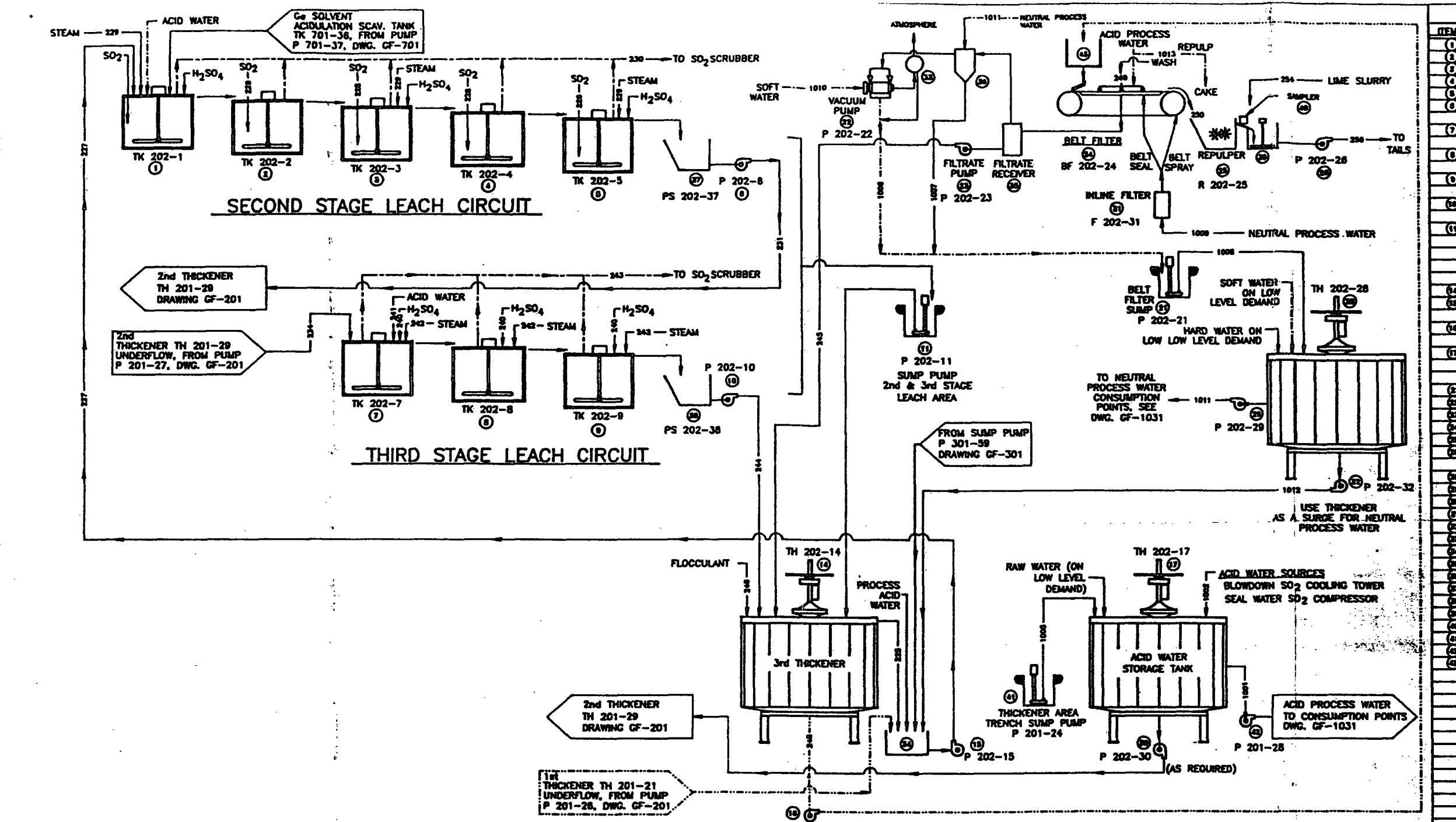




THE CHARGE IS THE PROPERTY OF
ECLA MINING COMPANY
WHICH IS FURNISHED FOR THE SOLE USE OF
EXPLORATION AND ACQUISITION OF TITLES
UPON AN AGREEMENT THAT IT WILL NOT BE
TRANSFERRED OR USED TO ANY OTHER
PURPOSES UNLESS FURNISHED
RIGHT UNDER CONTRACT PROVISIONS AND
PAYMENT OF FEES AS PROVIDED.

PROJECT AREA 200





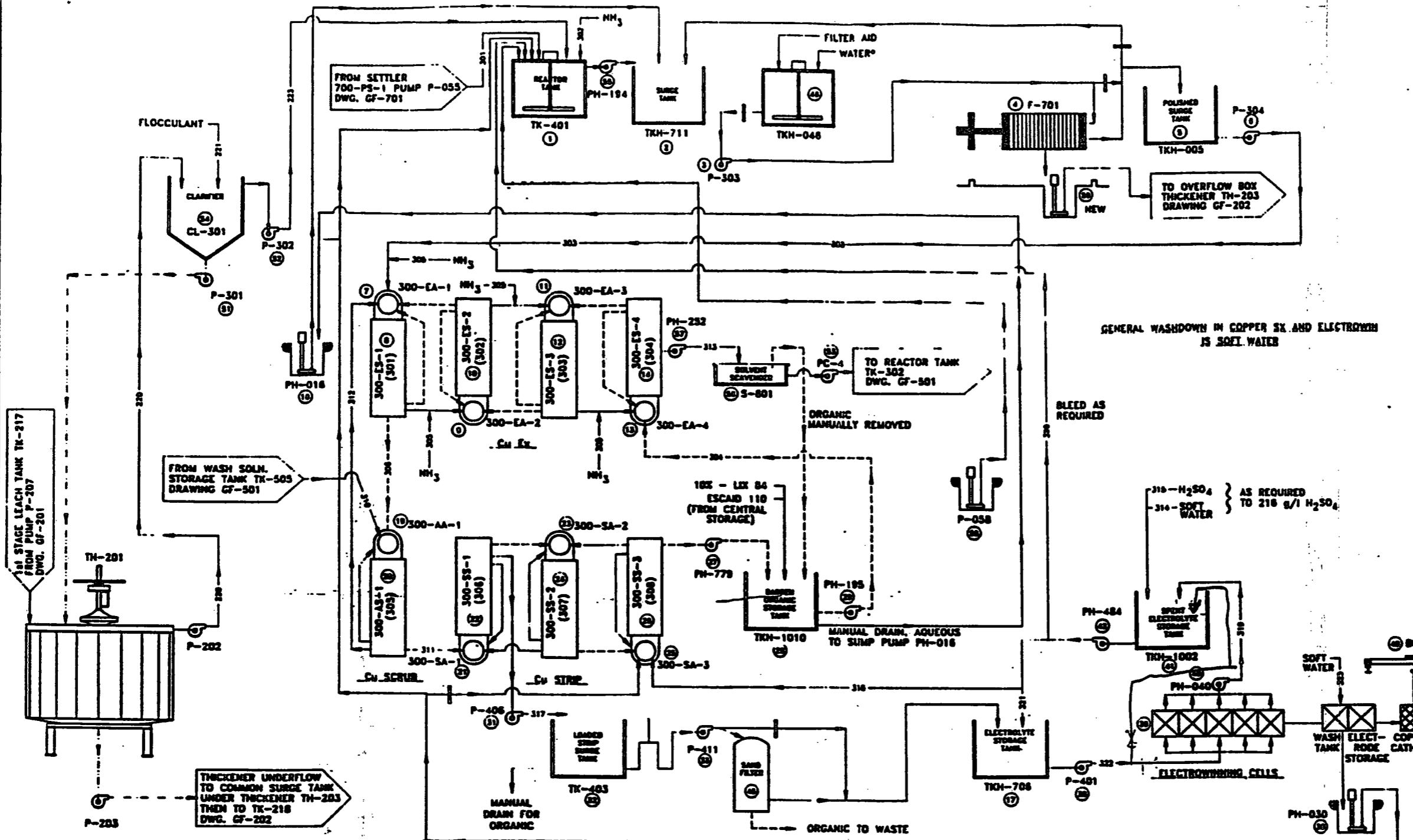
EQUIPMENT LIST		
ITEM	H.P.	DESCRIPTION
①	7.5	TANK 8'W x 12'H W/AGITATOR
②	7.5	TANK 8'W x 12'H W/AGITATOR
③	7.5	TANK 8'W x 12'H W/AGITATOR
④	7.5	TANK 8'W x 12'H W/AGITATOR
⑤	7.5	TANK 8'W x 12'H W/AGITATOR
⑥	5	2" x 1/2" GALLON TRANSFER PUMP
⑦	7.5	TANK 8'W x 8'H W/AGITATOR
⑧	7.5	TANK 8'W x 8'H W/AGITATOR
⑨	5	TANK 8'W x 8'H W/AGITATOR
⑩	5	2" x 1/2" GALLON TRANSFER PUMP
⑪	5	1 1/2" GALLON SUMP PUMP
⑫	3	20" x 10" EMCO THICKENER
⑬	3	2" x 1 1/2" GALLON
⑭		OVERFLOW PUMP
⑮	AIR	3" x 2" DORR UNDERFLOW PUMP
⑯	1	20" x 10" EMCO THICKENER
⑰	5	2" DURCO PUMP, SELF PRIME
⑱	35	CL1002 NASH
⑲	2	1-1/2" EMCO FILTRATE PUMP
⑳	1	9m ² DEXKOR BELT FILTER
㉑	5	REPULPER
㉒	5	1 1/2" GALLON SUMP PUMP
㉓	2	20" x 10" EMCO THICKENER
㉔	10	2" GOULD'S PUMP
㉕	AIR	3" x 2" DORR UNDERFLOW PUMP
㉖	-	INLINE FILTER
㉗	AIR	3" x 2" DORR UNDERFLOW PUMP
㉘	SEPARATOR (NASH)	
㉙	T	COLLECTION TANK
㉚		FILTRATE RECEIVER
㉛		SCRUBBER (DEXKOR)
㉜		PUMP SUMP
㉝		PUMP SUMP
㉞	115V	SUMP (TAILINGS)
㉟	5	1 1/2" GALLON SUMP PUMP
㉟	3	1 1/2" x 1" GOULD'S PUMP
㉟		SURGE TANK 3'W x 3'
㉟		TK 202-

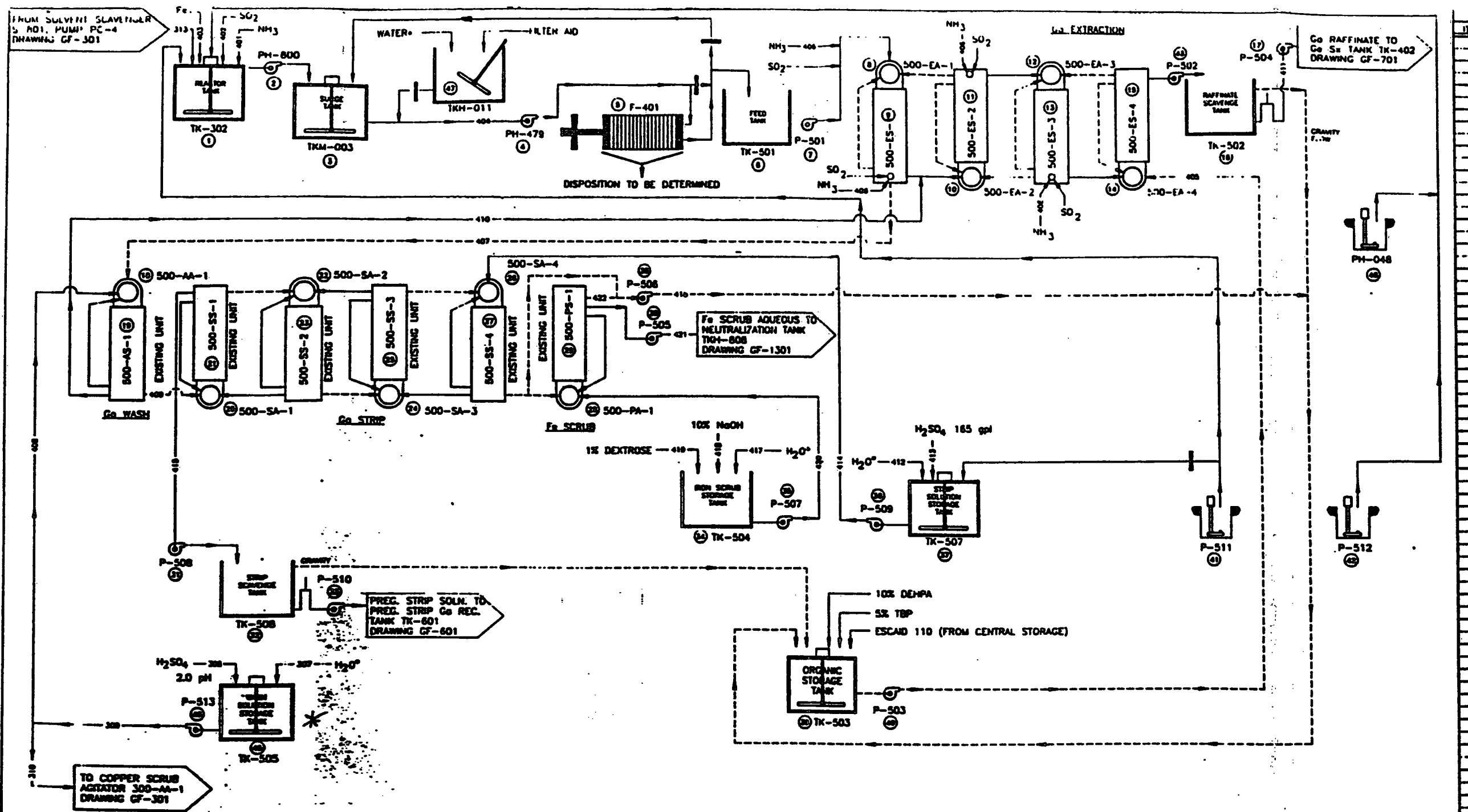
STREAM NUMBER	PHASE	SOLIDS PPM	LIQUID PPM	TOTAL PPM	WATER PPM	S.C.	TEMP. °F	H ₂ SO ₄ PPM	SO ₂ %
223 3rd THICKENER OVERFLOW	Liquid	-	18,222	-	18,222	16.6	1.20	116	204
227 FEED - 2nd STAGE LEACH	SOLID	4,673	15,597	-	14,260	34.8	1.32	134	127
228 SULFUR DISCHARGE - 2nd STAGE	GAS	-	-	545	545	110 ppm	1.0	120	25-30
229 STEAM - 2nd STAGE	GAS	-	-	612	612	-	-	353	-
230 2nd STAGE "OFF-GAS"	GAS	-	-	713	713	360 ppm	-	170	1.5
231 2nd STAGE LEACH DISCHARGE	SOLID	3,828	21,177	-	25,005	36.2	1.31	170	94
1001 ACID PROCESS WATER	Liquid	-	12,000	-	12,000	25.3	1.0	70	0-10
124 2nd STAGE THICKENER UNDERFLOW	SOLID	3,828	3,828	-	7,655	8.4	1.0	145	64
1002 ACID PROCESS WATER SOURCES	Liquid	-	13,648	-	13,648	27.1	1.0	100	0-10
1010 VACUUM PUMP SEAL WATER	Liquid	-	10,000	-	10,000	20	1.0	70	-
1011 PROCESS WATER (NEUTRAL)	Liquid	-	65,000	-	65,000	131.3	1.0	80	-
1012 NEUTRAL WATER THICKENER UNDERFLOW	SOLID	-	-	-	80	-	-	-	-
1013 CAKE REPULPER WATER	Liquid	-	4,631	-	4,631	6.3	1.0	70	0-10
1003 THICKENER AREA SUMP	SOLID	-	-	-	-	-	-	-	-
240 SULFURIC ACID 3rd STAGE	Liquid	-	2,188	-	2,188	2.4	1.0	70	93%
241 PROCESS WATER (ACID)	Liquid	-	350	-	350	0.7	1.0	70	0-10
242 STEAM - 3rd STAGE	GAS	-	-	650	650	-	-	353	-
243 3rd STAGE "OFF-GAS"	GAS	-	-	376	376	220 ppm	-	170	-
244 3rd STAGE LEACH DISCHARGE	SOLID	3,828	7,355	-	11,482	14.1	1.03	170	311
245 FILTRATE RETURN	Liquid	-	7,479	-	7,479	13.0	1.12	80	127
246 FLOCCULANT 3rd STAGE THICKENER	Liquid	-	187	-	187	0.4	1.0	70	-
248 3rd STAGE THICKENER UNDERFLOW	SOLID	3,828	4,908	-	8,736	11.2	1.36	140	204
249 FILTER WASH	Liquid	-	3,801	-	3,801	7.8	1.0	-	-
250 FILTER CAKE	SOLID	3,828	1,240	-	5,168	5.4	1.01	100	4.5
254 LIME SLURRY	SOLID	7	83	-	70	0.1	1.00	100	-
256 LEACH TAILINGS	SOLID	3,834	3,361	-	9,836	14.7	1.33	90	PH 7
1005 VACUUM PUMP SEAL WATER	Liquid	-	10,000	-	10,000	20	1.0	80	-
1007 VACUUM SYSTEM SCRUB WATER	Liquid	-	15,300	-	15,300	31	1.0	80	-
1008 RECYCLE PROCESS WATER	Liquid	-	54,328	-	54,328	108.7	1.0	80	-
1009 BELT SEAL/SPRAY WATER	Liquid	-	17,800	-	17,800	36.2	1.0	80	-

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CONSIDERED AN AGREEMENT THAT IT WILL NOT BE
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PROVIDED TO RECIPIENT UNDER CONTRACT PROVISIONS AND
SHELL OWNERSHIP THE PROPERTY OF HECLA MINING
COMPANY SUBJECT TO RECIPIENT OWN REQUIREMENTS.

ITEM	DESCRIPTION	REV.	DATE	APPROVED BY	APPROVED BY	APPROVED BY	APPROVED BY
GF-201	FIRST STAGE LEACH CIRCUIT FLOW DIAGRAM						
GF-301	Cu SOLVENT EXTRACTION CIRCUIT FLOW DIAGRAM						
APX PROJECT AREA 200							
2nd & 3rd STAGE LEACH CIRCUIT FLOW DIAGRAM							
HECLA							
MINING COMPANY							



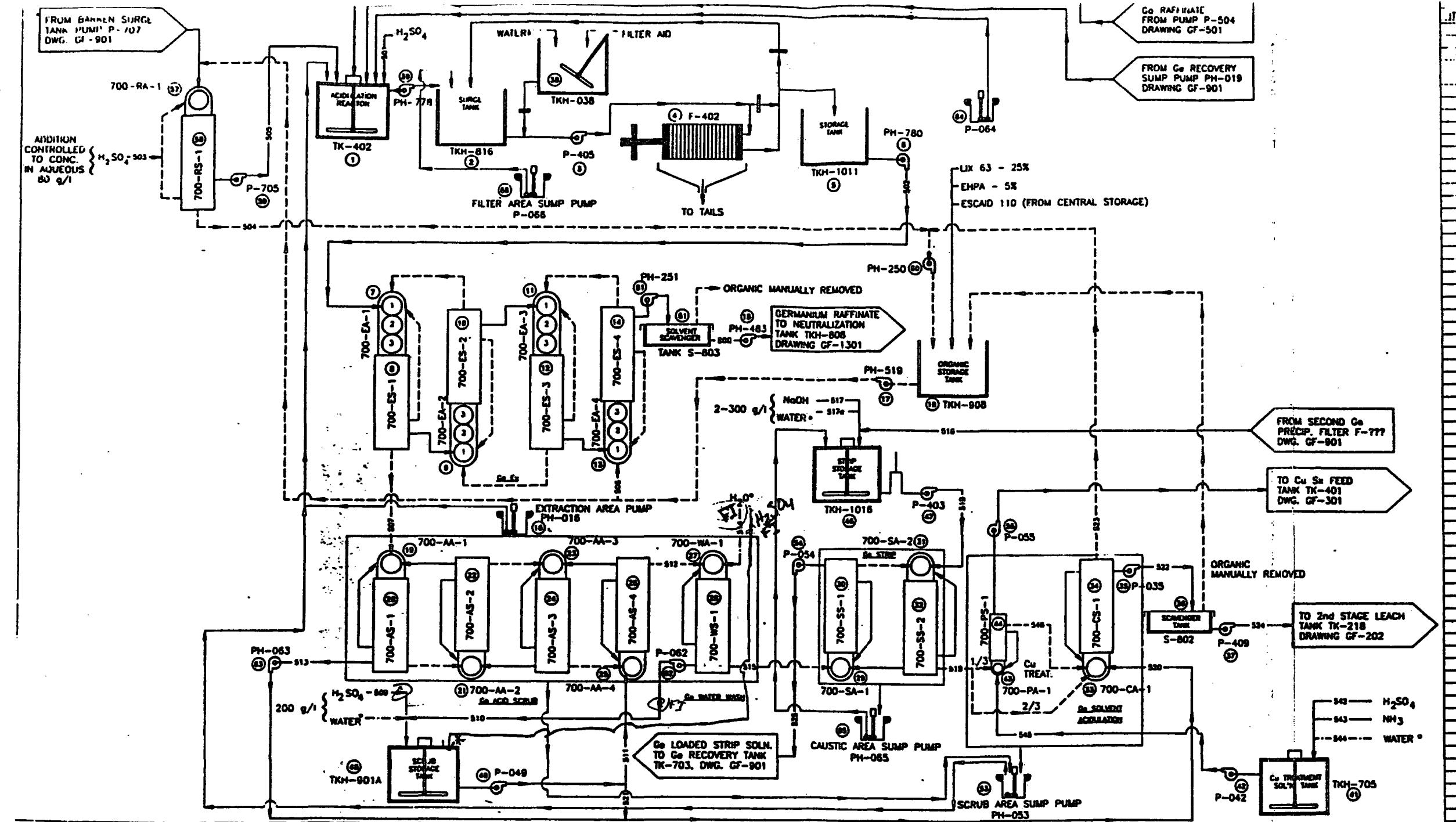




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THEIR OWN AND ACCEPTANCE OF SAME.
BY AN AGREEMENT THIS IS TO BE USED EX-
CLUSIVELY IN REFERENCE OR USE TO ANY OTHER
MOUNTAIN PARK COMPANY MACHINERY PURCHASED
BY LA MINING COMPANY PROVIDED THAT
THIS STAMPER IS NOT TO BE USED ON MACHINERY
BELONGING TO MOUNTAIN PARK COMPANY
EXCEPT TO REMOVE THEM FROM SERVICE.

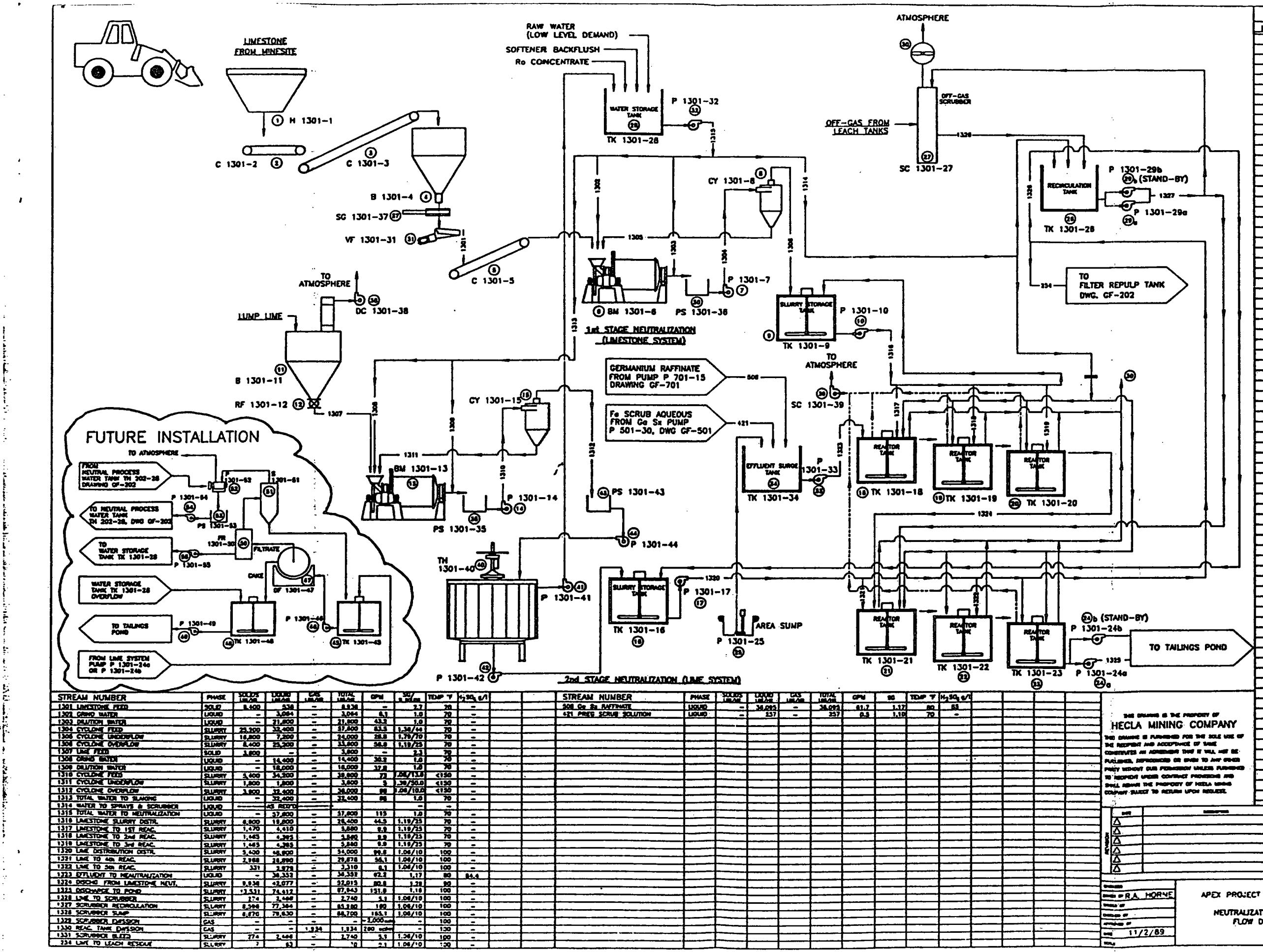
EXXON PROJECT AREA 500

SOLVENT EXTRACTION CIRCUIT
FLOW DIAGRAM



STREAM NUMBER	PHASE	SOLIDS PPM	LIQUID MM	GAS MM	TOTAL MM	CPW	SC	TEMP °F	MWSO OUT
411 CALCIUM SULFATE	LIQUID	-	33,572	-	33,572	80.0	1.12	60	4.6
501 SULFURIC ACID	ACID	-	2,323	-	2,323	2.0	1.06	70	0.35
502 GERMANIUM Si FEED	LIQUID	-	34,935	-	34,935	0.7	1.16	60	0.4
503 ACID TO ORGANIC RECOVERY	LIQUID	-	130	-	130	0.2	1.00	70	0.35
504 RECOVERED ORGANIC	LIQUID	-	163	-	163	0.4	0.85	60	245
505 RECOVERY AQUEOUS	LIQUID	-	900	-	900	1	1.30	60	125
506 BARIUM SOLVENT	LIQUID	-	5,103	-	5,147	19.2	0.85	70	20
507 LEACHED ORGANIC	LIQUID	-	8,147	-	8,147	19.2	0.85	60	11
508 Ge Si RAFTMADE	LIQUID	-	34,093	-	34,093	51.7	1.17	60	0.35
509 SULFURIC ACID TO SCRUB EQLN	LIQUID	-	446	-	446	0.5	1.00	70	0.35
510 SPENT WATER SCRUB	LIQUID	-	1,223	-	1,223	2.4	1.0	60	-
511 SOLUTION TO ACID SCRUB	LIQUID	-	1,515	-	1,515	2.7	1.12	70	202
512 ACID SCRUBBED SOLVENT	LIQUID	-	8,147	-	8,147	19.2	0.85	60	11
513 ACID SCRUB PRODUCT	LIQUID	-	1,515	-	1,515	2.7	1.12	60	202
514 WATER TO SOLVENT WASH	LIQUID	-	1,223	-	1,223	2.4	1.0	70	-
515 WATER WASHED SOLVENT	LIQUID	-	8,147	-	8,147	19.2	0.85	60	11
516 2nd PRECIPITATE FILTRATE	LIQUID	-	434	-	434	0.6	1.00	60	-
517 H2O TO STRIP SOLUTION	LIQUID	-	269	-	269	0.4	1.53	70	-
517a WATER TO STRIP SOLUTION	LIQUID	-	72	-	72	0.1	1.0	70	-
518 STRIP SOLUTION	LIQUID	-	765	-	765	1.3	1.10	70	-
519 STRIPPED SOLVENT	LIQUID	-	7,564	-	7,564	10	0.85	60	-
520 AQUEOUS TO ACIDULATION	LIQUID	-	2,324	-	2,324	4.3	1.12	60	202
521 ACIDSCRUB SOLUTION TO ACID	LIQUID	-	609	-	609	1.5	1.12	60	202
522 ACIDULATION AQUEOUS	LIQUID	-	2,324	-	2,324	4.3	1.12	60	150
523 ACIDULATED SOLVENT	LIQUID	-	7,564	-	7,564	10	0.85	60	150
524 SCAVENGER AQUEOUS TO LEACH	LIQUID	-	2,324	-	2,324	4.3	1.12	60	150
525 PRODUCT STRIP SOLUTION	LIQUID	-	767	-	767	1.4	1.10	60	-
526 H2SO4 TO PURF. SOLUTION	LIQUID	-	34.2	-	34.2	0.04	1.00	70	0.35
543 NH3 TO PURF. SOLUTION	LIQUID	-	34.2	-	34.2	0.07	1.0	70	-
544 WATER TO PURF. SOLUTION	LIQUID	-	100	-	100	0.4	1.0	70	-
545 COPPER PURIFYING SOLUTION	LIQUID	-	282	-	282	0.5	1.05	70	-
546 ORGANIC FROM PURIFICATION	LIQUID	-	2,974	-	2,974	7.0	0.85	70	-

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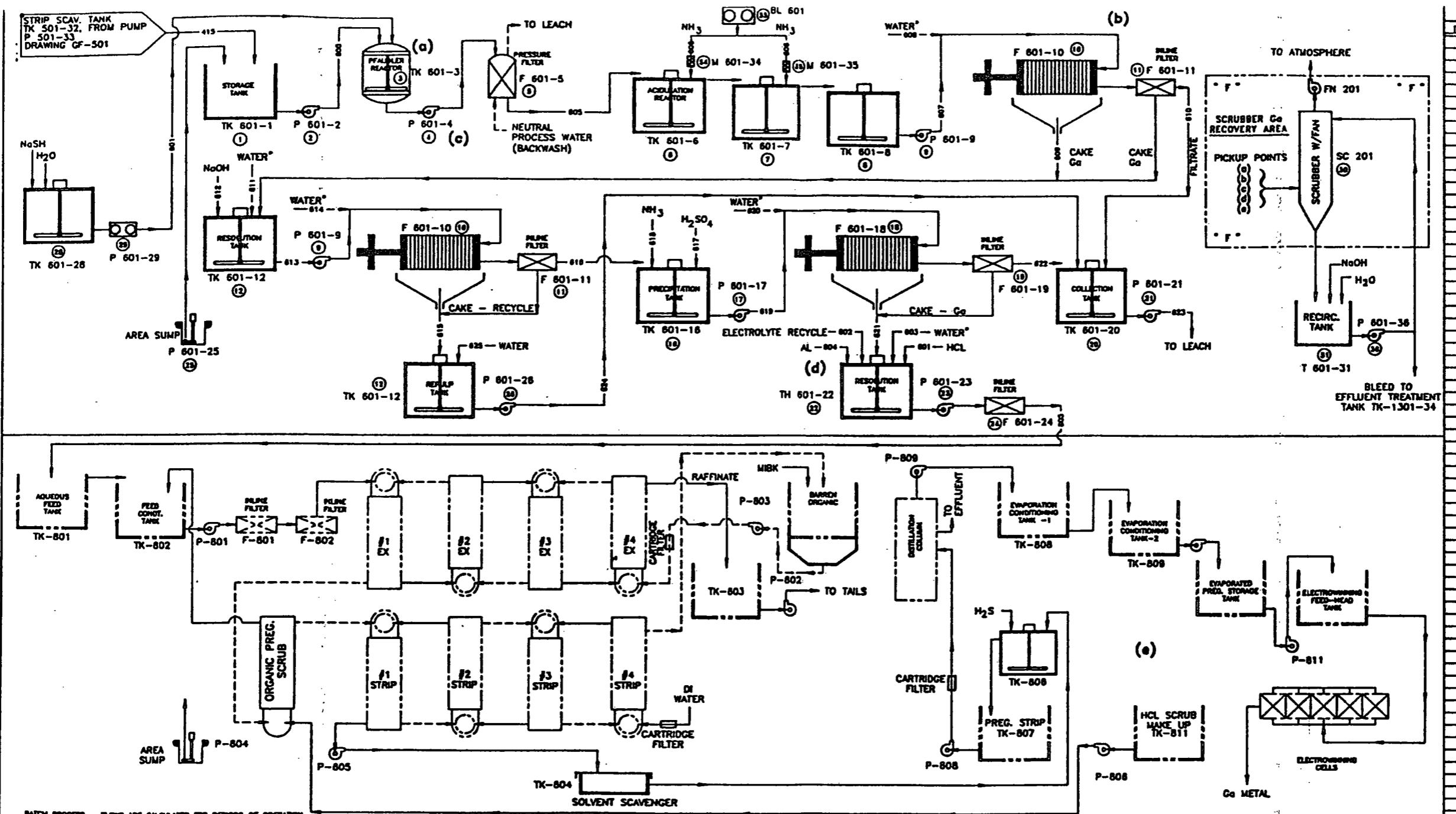


EQUIPMENT LIST			
E.M.	H.P.	DESCRIPTION	ECN
1		3 YD ³ FEED HOPPER	H 13
2	3	24" x 8' BELT FEEDER	C 13
3	5	18" x 84'L BELT CONVEYOR	C 13
4		230 TON LIMESTONE STORAGE BIN	B 13
5		16" x 26'L BELT CONVEYOR	C 13
6	50	5'W x 5'H EMCO BALL MILL	BM 1
7	10	1 1/2" CALCHER PUMP	P 13
8		3' KREBS HYDROCYCLONE	CY 1
9	5	TANK 8'W x 8'H R.L. SLURRY STORAGE	TK 13
10	5	1 1/2" CALCHER PUMP	P 13
11		200 TON LUMP LIME STORAGE BIN	B 13
12	2	6" ROTARY FEEDER	RF 13
13	10	30" x 36" DENVER BALL MILL	BM 1
14	10	1 1/2" CALCHER PUMP	P 13
15		3' KREBS HYDROCYCLONE	CY 1
16	5	TANK 8'W x 8'H WS W/AGITATOR SLURRY STORAGE	TK 13
17	10	1 1/2" CALCHER PUMP	P 13
18	3	12'W x 15'H REACTOR W/AGITATOR	TK 13
19	2	10'W x 10'H FRP REACTOR WITH AGITATOR	TK 13
20	2	10'W x 10'H FRP REACTOR WITH AGITATOR	TK 13
21	2	8'W x 12'H REACTOR W/AGITATOR 3' FALSE BOTTOM	TK 13
22	2	8'W x 8'H FRP REACTOR	TK 13
23	2	8'W x 8'H FRP REACTOR	TK 13
24	7.5	3" x 2" GOULDS PUMP	P 13
25	7.5	3" x 2" GOULDS PUMP	P 13
26	5	1 1/2" CALCHER SUMP PUMP	P 13
27		7W x 7H RECIRCULATION TANK	TK 1
28	10	OFF-GAS SCRUBBER	SC 1
29	-	TANK 7W x 8'H FRP WATER STORAGE	TK 1
30	10	2" CALCHER PUMP	P 13
31	10	2" CALCHER PUMP	P 13
32	10	SCRUBBER FAN (FURNISHED WITH SCRUBBER)	
33		VIBRATING FEEDER	VF 13
34	10	2" GOULDS PUMP - IRON	P 13
35	1.5	1" GOULDS PUMP	P 13
36	3	12'W x 14'H FRP SURGE TANK	TK 13
37		PUMP SUMP	PS 1
38		PUMP SUMP	PS 1
39		SLIDE GATE	SG 1
40		BIN MOUNT DUST COLLECTOR	DC 1
41		EXIST. 3 STAGE SCRUB. EXHAUST	SC 1
42	2	THICKENER 20" x 12'	TH 1
43	5	2" x 1 1/2" CALCHER PUMP	P 13
44	AIR	3" x 2" DORR PUMP	P 13
45		PUMP SUMP	PS 1
46		PUMP	P 13
47		FUTURE TANK WITH AGITATOR	TK 1
48		FUTURE PUMP	P 13
49		FUTURE FILTER	DF 1
50		FUTURE TANK WITH AGITATOR	TK 1
51		FUTURE PUMP	P 13
52		FUTURE FILTRATE RECEIVER	FR 1
53		FUTURE BAROMETRIC SEPARATOR	S 13
54		FUTURE VACUUM PUMP	P 13
55		FUTURE SUMP PUMP	PS 1
56		FUTURE PUMP	P 13
57		FUTURE PUMP	P 13

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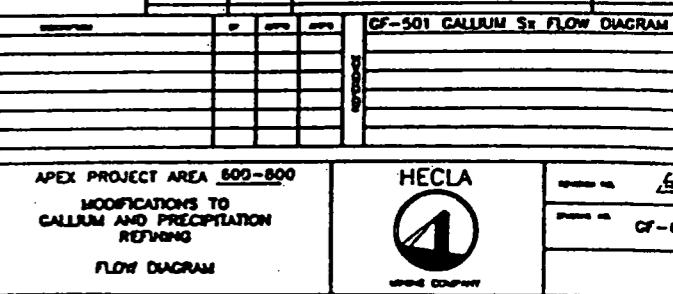
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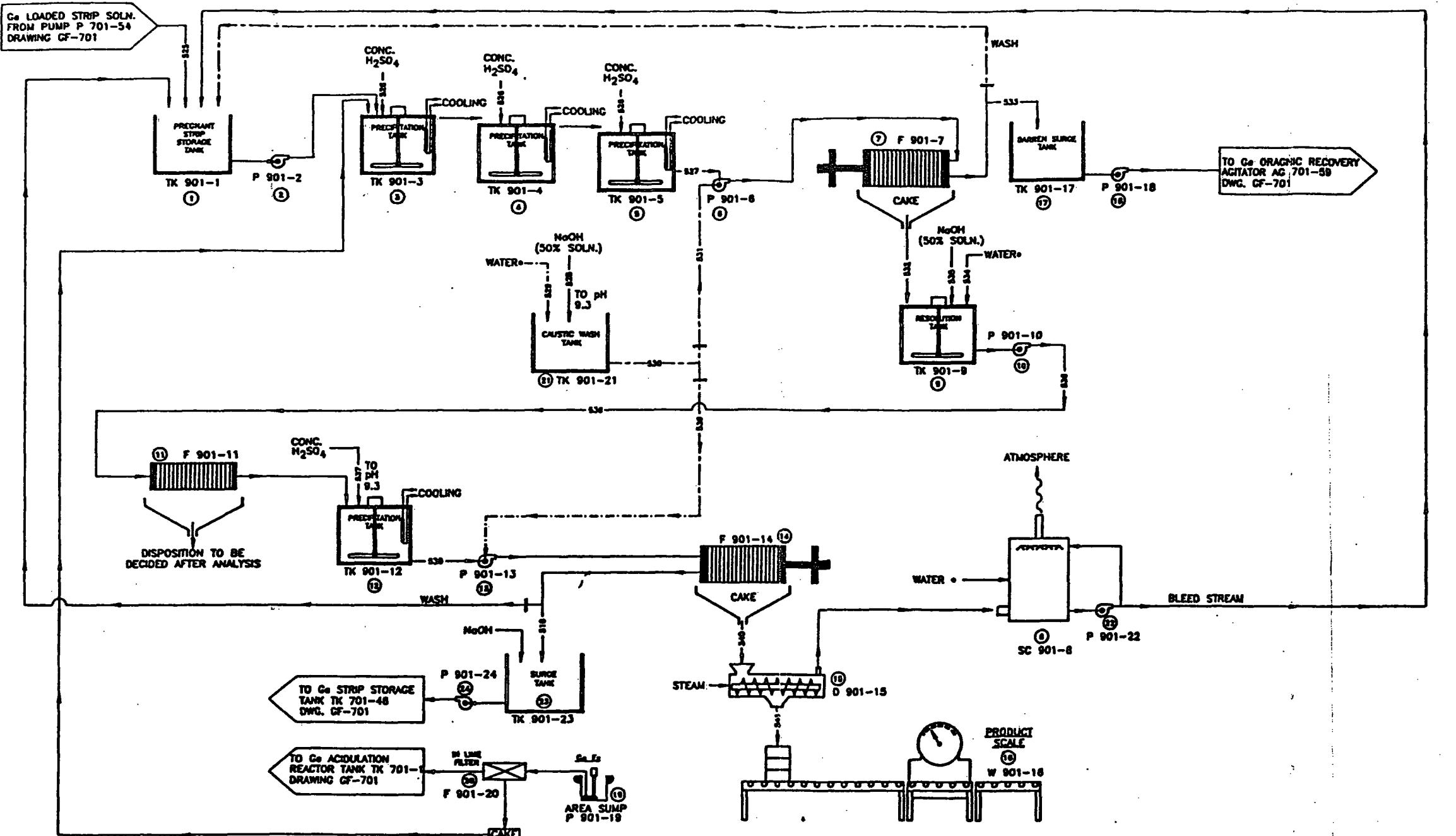
A. MORNE	APPEX PROJECT AREA 1300			HECLA MINING COMPANY	OF-13
1/2/89	NEUTRALIZATION SYSTEM FLOW DIAGRAM				



BATCH PROCESS - FLOWS ARE CALCULATED FOR PERIODS OF OPERATION												
STREAM NUMBER	PHASE	DURATION	SOLID kg/hr	Liquid kg/hr	Gas kg/hr	Total kg/hr	OPM	SS	TEMP °F	H ₂ SO ₄ g/l	MgCl ₂ g/l	NaCl g/l
415 PREGNANT STRIP SOLUTION	LIQUID	CONT.	-	902	-	902	1.1	1.10	60	74	-	-
600 FEED TO GALLIUM RECOVERY	LIQUID	0 hr/24	-	4,638	-	4,638	0.8	1.10	60	74	-	-
601 SODIUM HYDROXIDE	LIQUID	0 hr/24	-	72	-	72	0.1	1.20	70	-	40	-
602			-	-	-	-	-	-	-	-	-	-
603 SULFIDE FILTRATE	LIQUID	0 hr/24	-	3,000	-	3,000	0.1	1.1	60	-	-	-
605 AMMONIA	LIQUID	0 hr/24	-	240	-	240	0.5	1.0	70	-	-	-
607 GALLIUM - IRON PRECIPITATE	SLURRY	6 hr/24	120	3,000	-	3,120	0.3	1.12	60	-	-	-
608 WASH WATER	LIQUID	20 min	-	810	-	810	20	1.0	70	-	-	-
609 GALLIUM/IRON FILTER CAKE	SOLID	-	120	305	-	425	-	1.20	60	-	-	-
610 GALLIUM/IRON FILTRATE	LIQUID	0 hr/24	-	5,440	-	5,440	0.8	1.11	60	-	-	-
611 REFLUX WATER	LIQUID	10 min	-	153	-	153	10	1.0	70	-	-	-
612 SODIUM HYDROXIDE	LIQUID	15 min	-	165	-	165	5	1.53	70	-	-	-
613 RELEASED PULP	SLURRY	0 hr/24	40	731	-	771	1.2	1.24	60	-	-	-
614 WASH WATER	LIQUID	15 min	-	200	-	200	10	1.0	70	-	-	-
615 IRON FILTER CAKE	SOLID	0 hr/24	40	96	-	136	-	1.25	60	-	-	-
616 GALLIUM FILTRATE	LIQUID	0 hr/24	-	876	-	876	1.5	1.21	60	-	-	-
617 SULFURIC ACID	LIQUID	0 hr/24	-	273	-	273	1.7	1.00	70	-	-	-
618 AMMONIA	LIQUID	1 hr	-	32	-	32	0.4	1.0	70	-	-	-
619 GALLIUM HYDROXIDE PRECIPITATE	SLURRY	1 hr	104	1,043	-	1,147	1.0	1.2	70	-	-	-
620 WASH WATER	LIQUID	0 hr/24	-	474	-	474	11	1.0	70	-	-	-
621 GALLIUM HYDROXIDE CAKE	SOLID	30 min	104	241	-	344	-	1.25	70	-	-	-
622 GALLIUM HYDROXIDE FILTRATE	LIQUID	0 hr/24	-	1,318	-	1,318	2.2	1.18	70	-	-	-
623 RECycles TO ORE LEACH	SLURRY	1 hr	240	41,500	-	41,740	3	1.13	70	-	-	-
624 REFLUXED IRON CAKE	SLURRY	10 min	40	180	-	200	12	1.18	70	-	-	-
625 IRON CAKE REFLUX WATER	LIQUID	3 min	-	84	-	84	10	1.0	70	-	-	-
601 HYDROCHLORIC ACID	LIQUID	1 hr	-	819	-	819	6.4	1.10	70	-	-	383
602 ELECTROLYTE RECYCLE	LIQUID	1 hr	-	9	-	9	-	1.11	7	-	-	-
603 BATER	LIQUID	1 hr	-	540	-	540	0.5	1.0	70	-	-	-
604 ALUMINUM	LIQUID	1 hr	3	-	-	3	-	2.7	70	-	-	-
605 WASH SOLVENT EXTRACTION FEED	LIQUID	-	-	370	-	370	4.1	1.11	70	-	-	140

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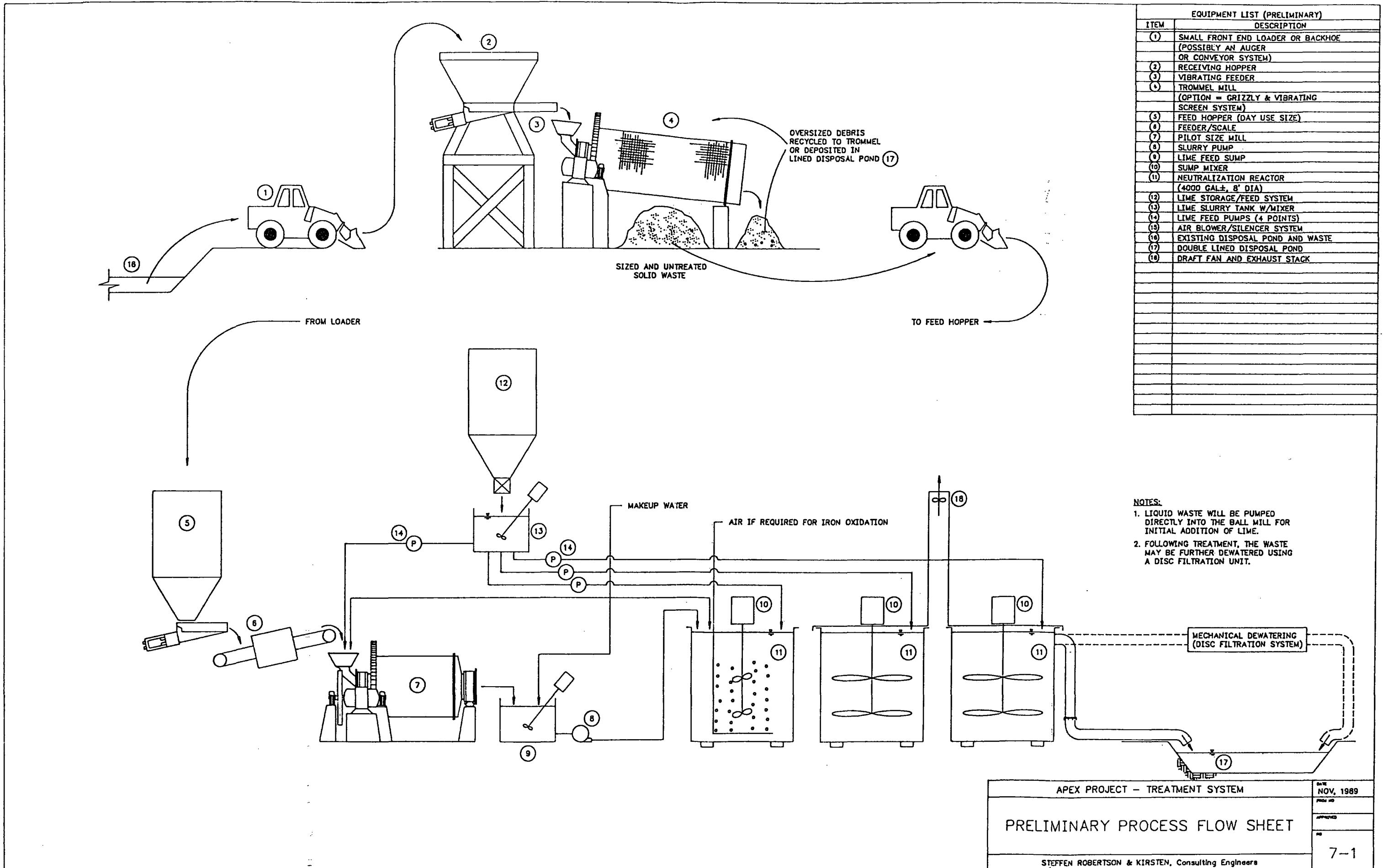
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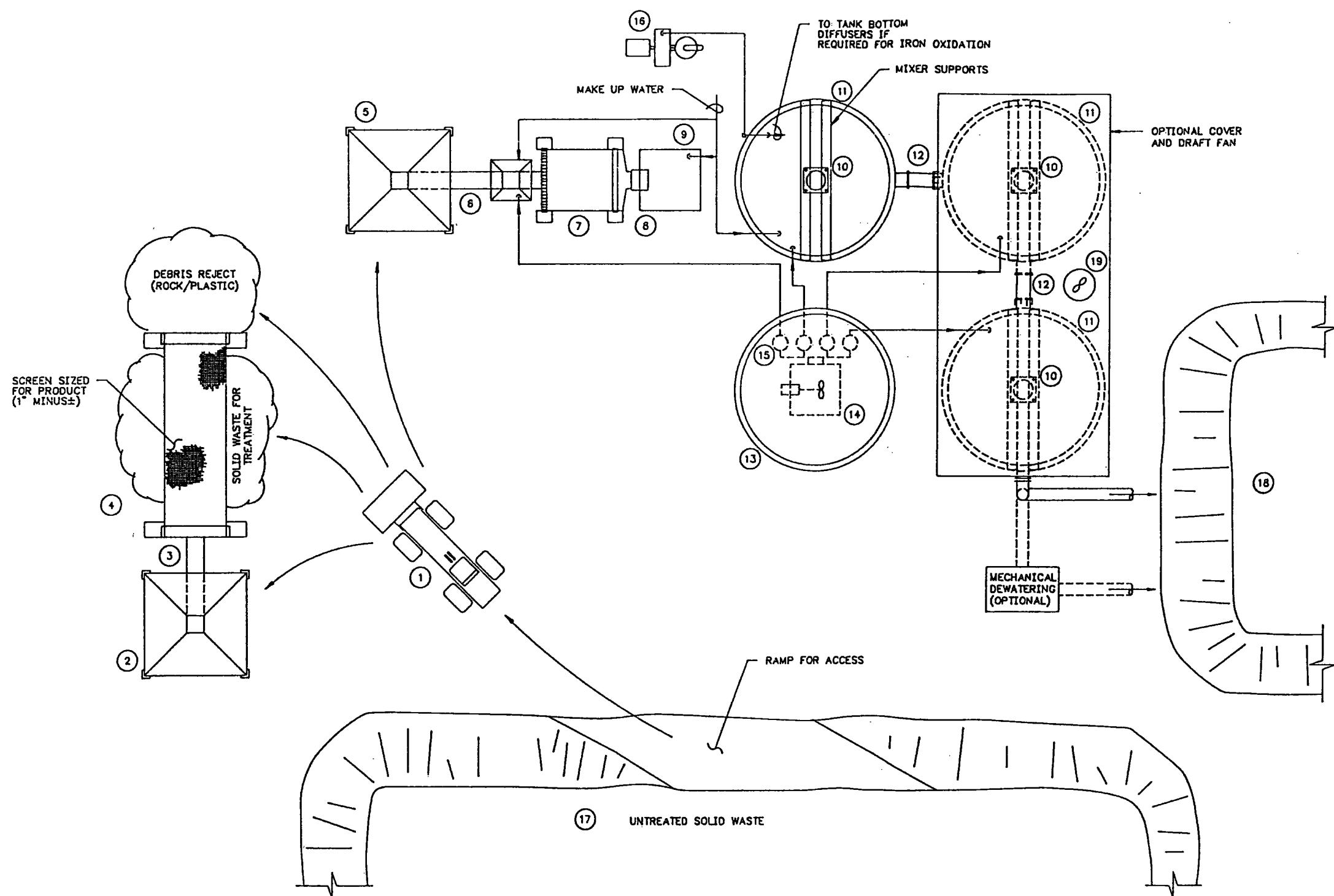


PROJECT AREA 900

**GERMANIUM RECOVERY
FLOW DIAGRAM**







TREATMENT SYSTEM PLAN VIEW

EQUIPMENT LIST (PRELIMINARY)	
ITEM	DESCRIPTION
(1)	SMALL FRONT END LOADER OR BACKHOE (POSSIBLY AN AUGER OR CONVEYOR SYSTEM)
(2)	RECEIVING HOPPER
(3)	VIBRATING FEEDER
(4)	TROMMEL MILL (OPTION = GRIZZLY & VIBRATING SCREEN SYSTEM)
(5)	FEED HOPPER (DAY USE SIZE)
(6)	FEEDER/SCALE
(7)	PILOT SIZE MILL
(8)	SLURRY PUMP
(9)	SLURRY TANK
(10)	SLURRY MIXER
(11)	NEUTRALIZATION TANK
(12)	INTERTANK PIPING W/FLEXIBLE HOSE
(13)	LIME STORAGE/FEED SYSTEM
(14)	LIME SLURRY TANK W/MIXER
(15)	LIME FEED PUMPS (4 POINTS)
(16)	AIR BLOWER/SILENCER SYSTEM
(17)	EXISTING STORAGE POND
(18)	DOUBLE LINED DISPOSAL POND
(19)	EXHAUST STACK AND FAN

NOTES:

- SECOND AND THIRD NEUTRALIZATION TANKS MAY BE COVERED AND VENTED WITH DRAFT FAN TO DISSIPATE AMMONIA.

APEX PROJECT - TREATMENT SYSTEM

DATE
NOV, 1989

GENERALIZED NEUTRALIZATION
TREATMENT SYSTEM

STEFFEN ROBERTSON & KIRSTEN, Consulting Engineers

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7-2